

BIOWKK Workshop Dortmund 2012

Open adsorption systems for thermal energy storage applications

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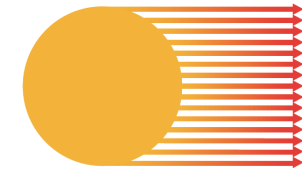
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Structure of ZAE Bayern



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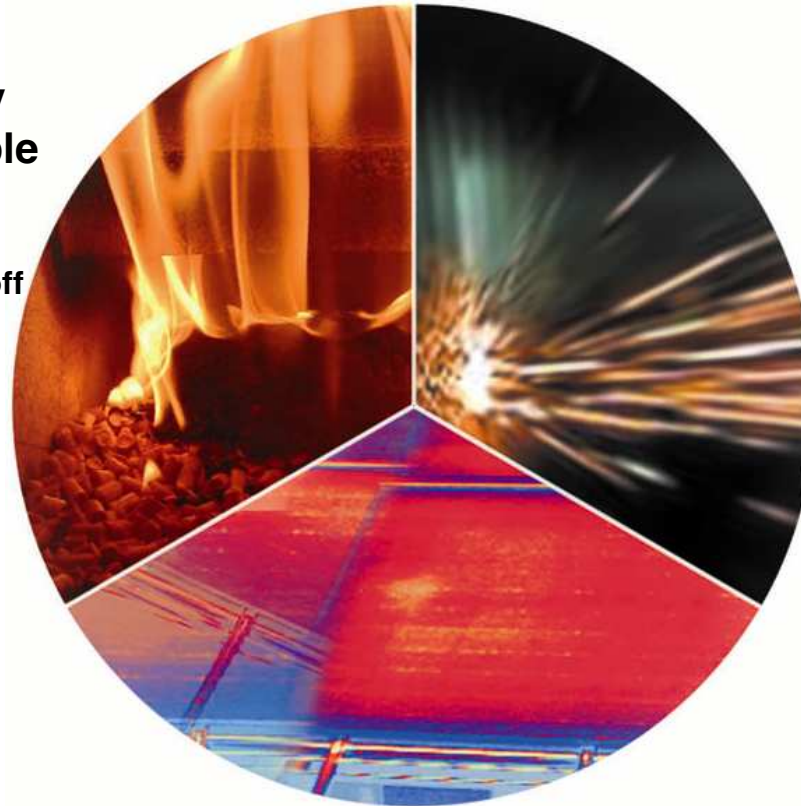
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2. Development
3. Examples
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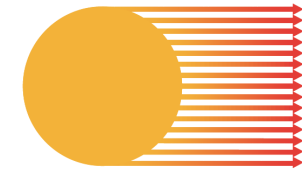
1. Introduction

1.1 Thermal Energy Storage Technologies

Sensible	Latent	Thermochemical
		
The energy storage density is defined by physics		
Specific heat capacity Temperature difference	Enthalpy of melting / Enthalpy of evaporating	Enthalpy of reaction
$\sim 40 - 80 \text{ kWh/m}^3$	$\sim 50 - 140 \text{ kWh/m}^3$	$\sim 80 - 300 \text{ kWh/m}^3$

1. Introduction

1.2 Classification of Sorption Heat Storage



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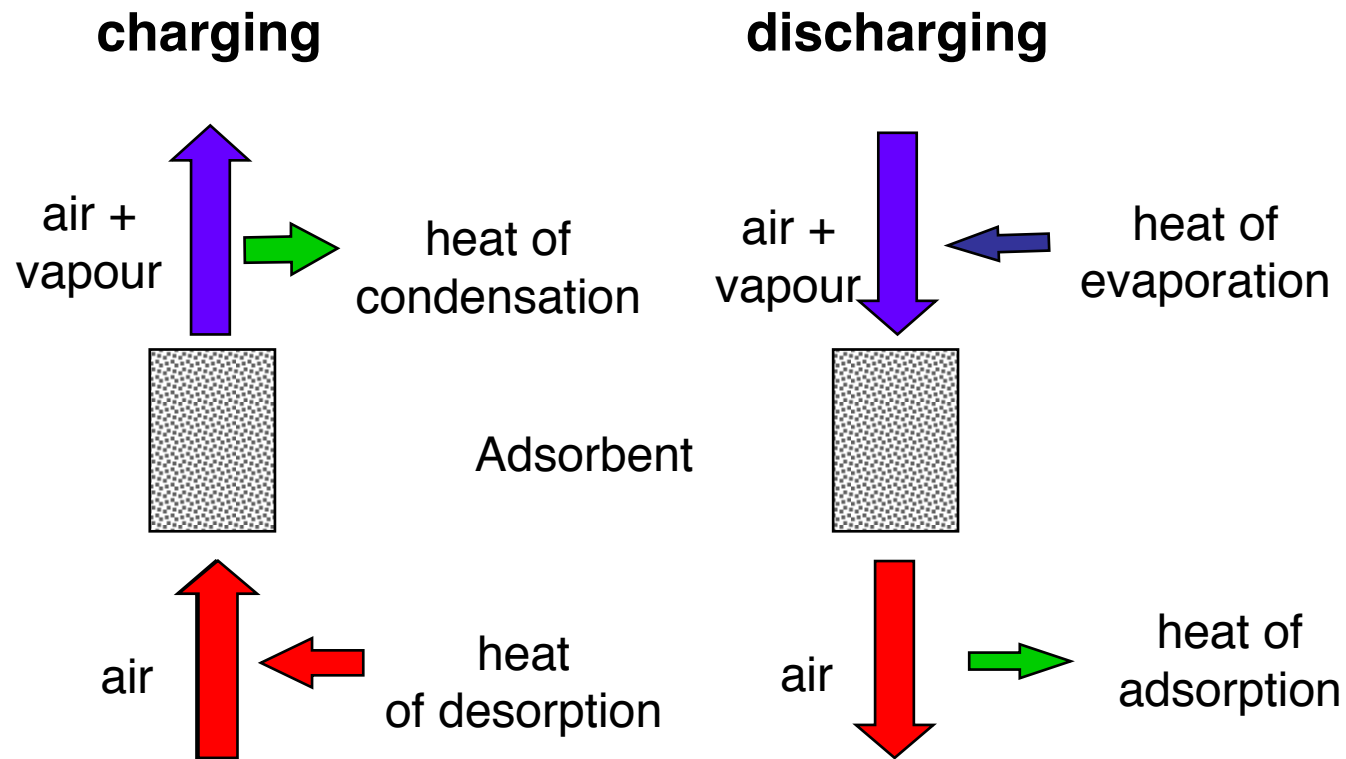
Thermochemical Heat Storage		
Reversible Chemical Reactions	Sorption	
	Absorption	Adsorption
Chemical Bindings (e.g. Covalence)	Solubility, Mixing without reaction	Interaction of molecules (e.g. van der Waals)
$Mg(OH)_2$ $MgO+H_2O$	LiBr / Water	Zeolite / Water

Characteristics of sorption heat storage:

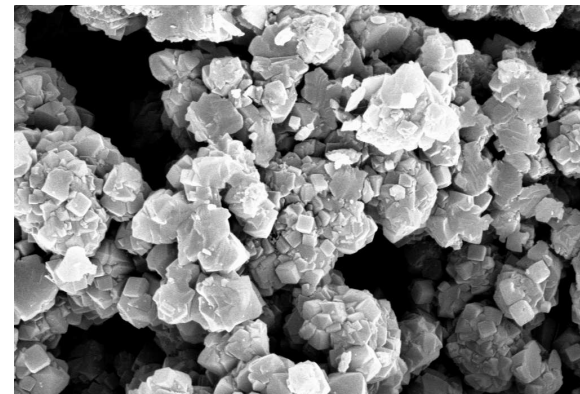
- Temperatures are not fixed
- Linked to the ambient

1. Introduction

1.3 Open Adsorption System

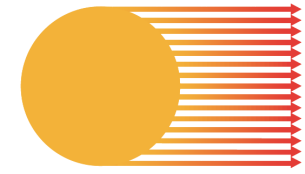


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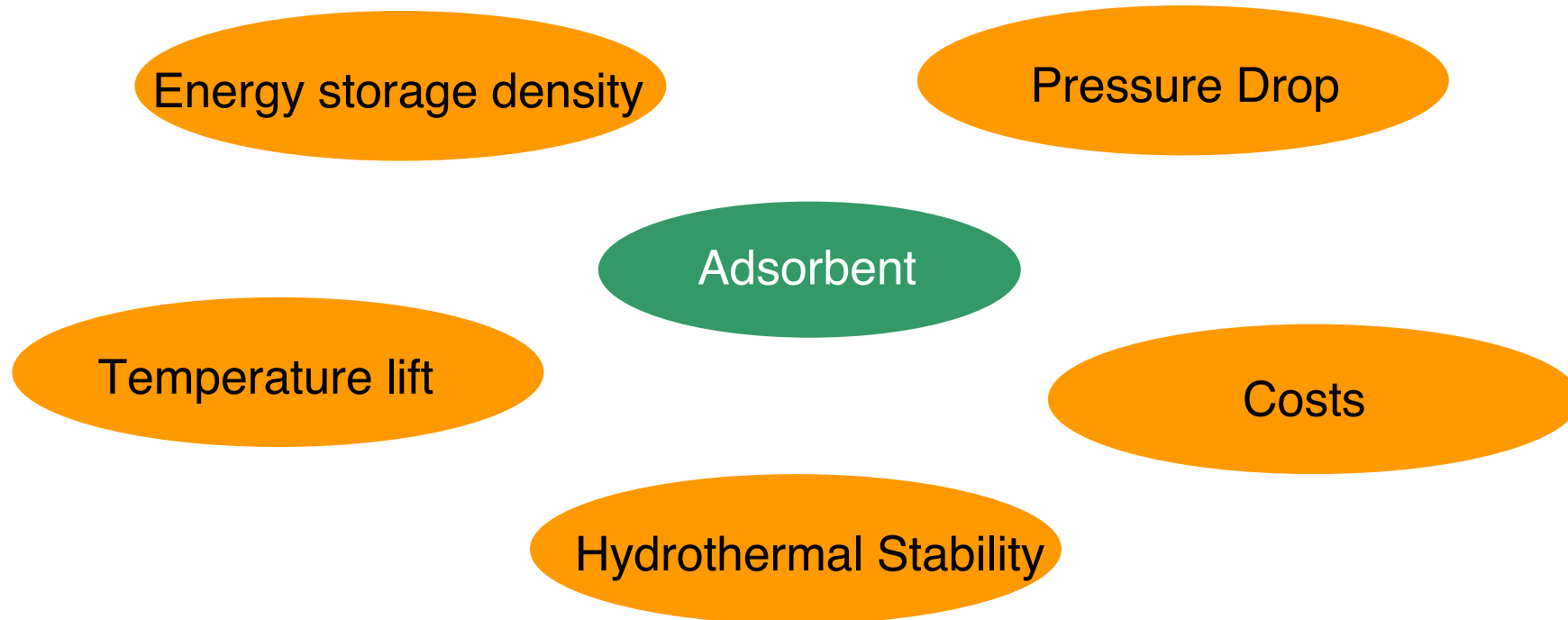


2. Development

2.1 Selection Criteria for Adsorbent Materials



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2. Development

2.2 Characterization of Adsorbent Materials

Equilibrium



Possible Energy Storage Capacity

Stability



Durability of the material

Transient

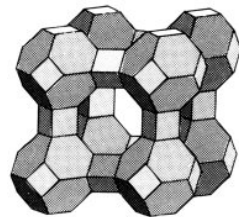


Performance

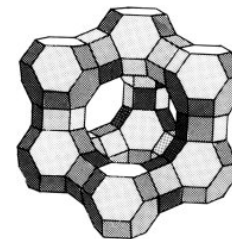
2. Development

2.3 Suitable Adsorbent Materials

Adsorbent	Water uptake / %	Temperatur lift	Stability	Costs / kg
Silicagel	35 - 50	☹	☺	☺ 0.5 - 2 €
Zeolite	20 - 35	☺	☺	☹ 2 - 10 €
ALPO / SAPO	35 - 50	?	?	☹
MOF	35 - 50	?	?	☹



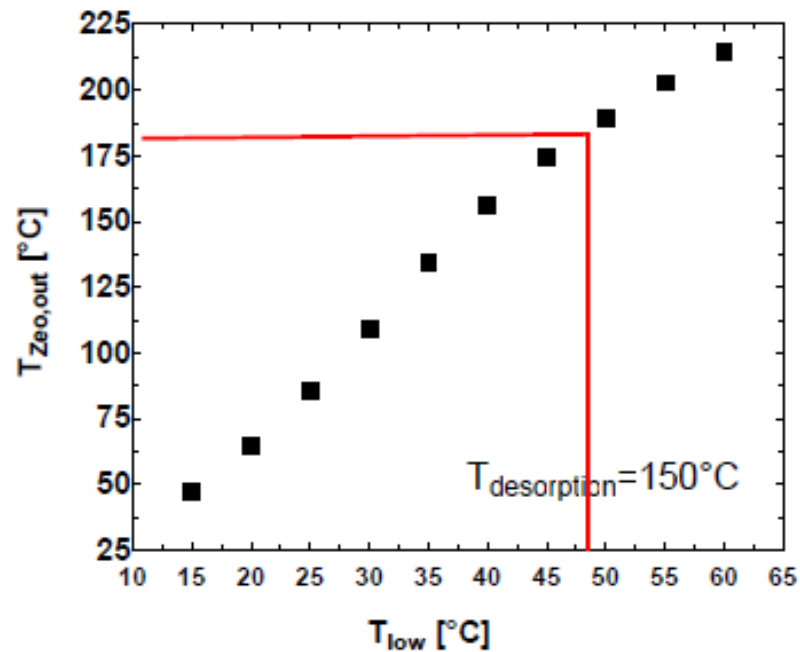
Zeolite A: 2,000,000 t/a



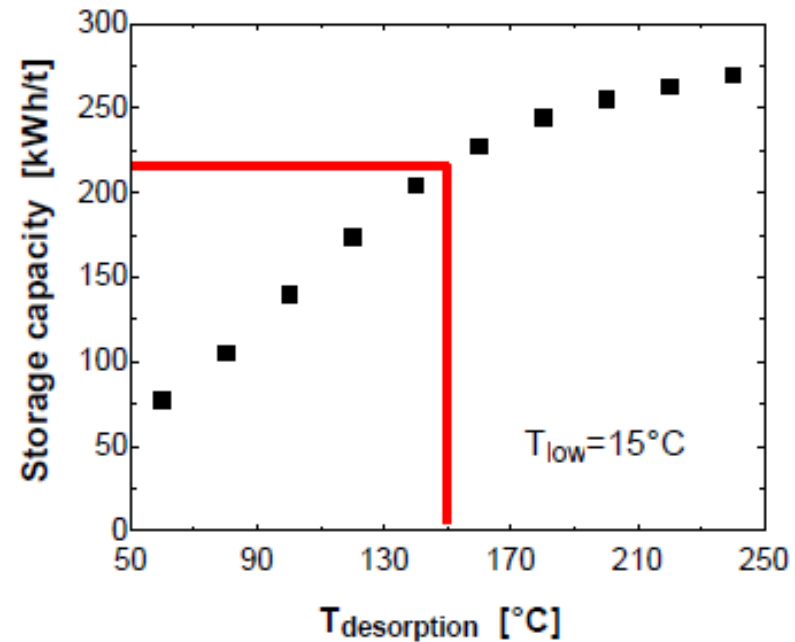
Zeolite X / Y: 100,000 t/a

2. Development

2.4 Boundary Conditions



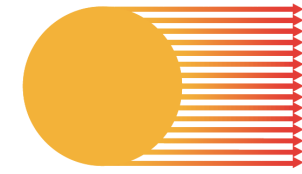
- Temperature lift depends on temperature of the inlet



- Storage capacity increases with higher temperatures of desorption

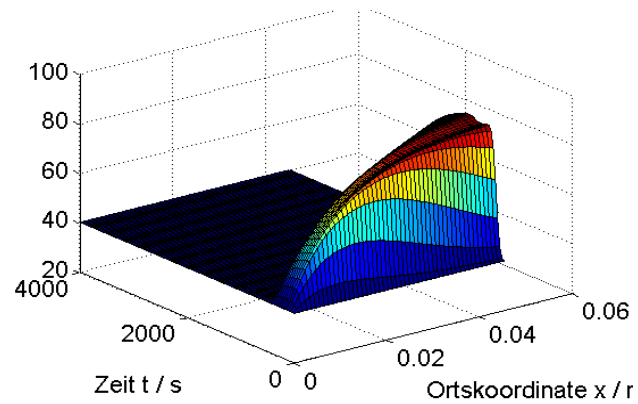
2. Development

2.5 Designing the Storage System

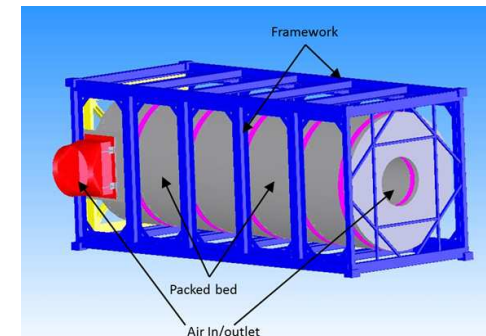


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Simulation



Computer Aided Design



Construction

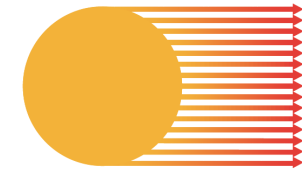


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3. Example

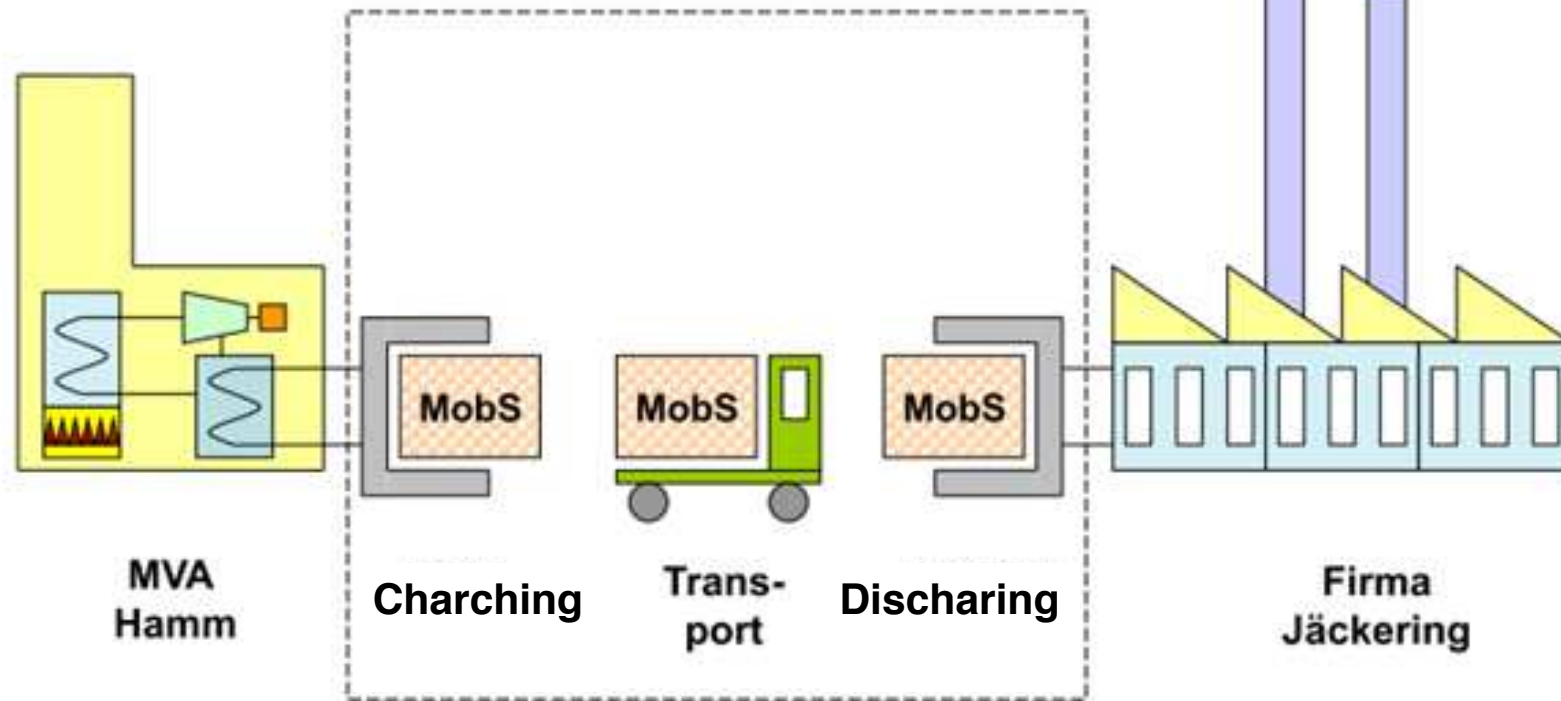
3.1 Mobile Sorption Heat Storage - Principle



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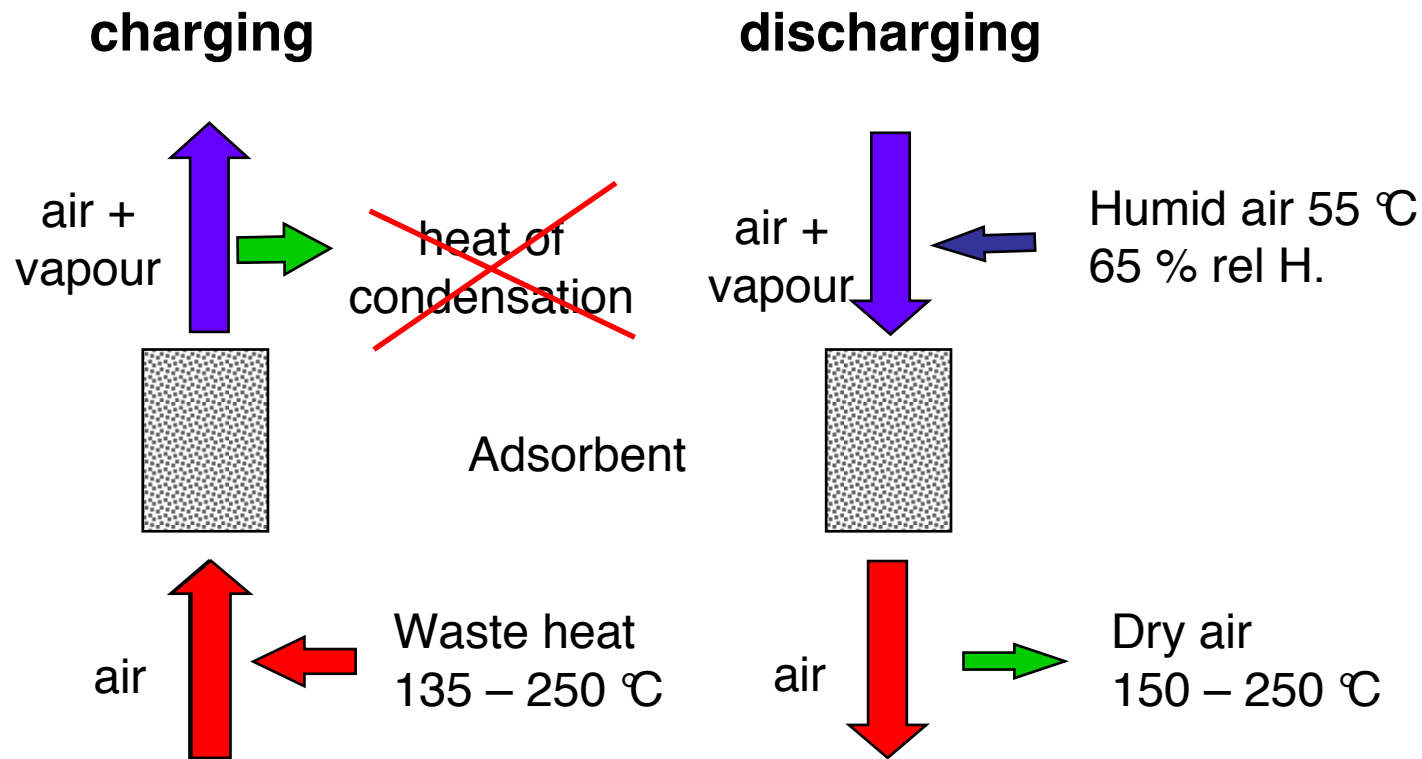
Waste Incinerator

Drying Process



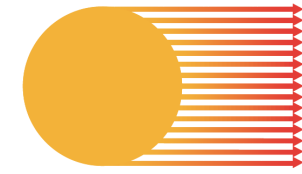
3. Example

3.2 Mobile Sorption Heat Storage - Conditions



3. Example

3.3 Mobile Sorption Heat Storage - Realization



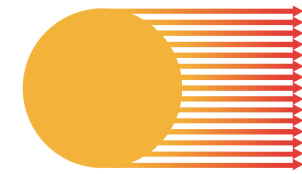
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- Length: 8.3 m
- Height: 2.9 m
- Zeolite: 14 t
- Energy “on the wheel”: up to 4 MWh

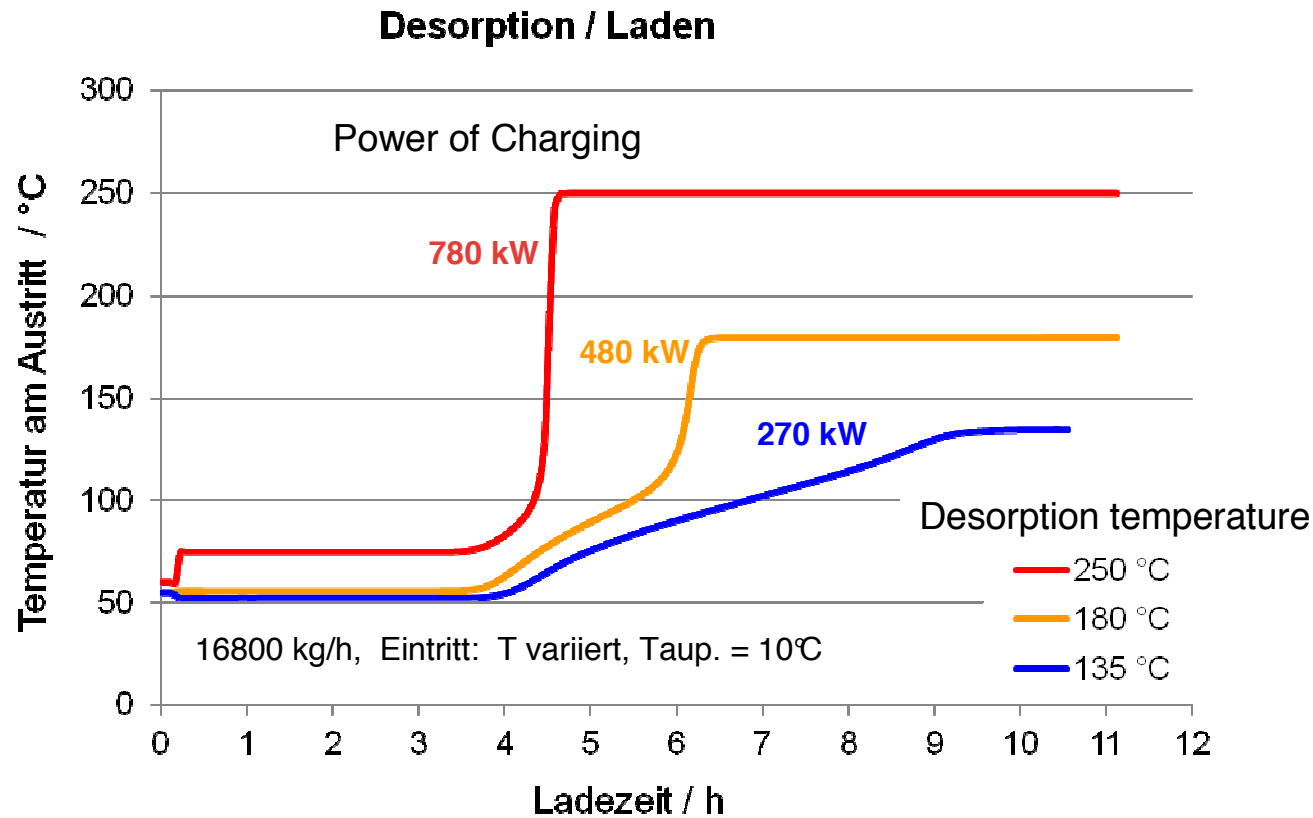


3. Example

3.4 Mobile Sorption Heat Storage - Simulation



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Simulated Data
for ideal fixed
bed

High desorption temperature:

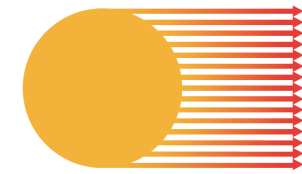
- Short time for charging
- High power of charging

Low desorption temperature:

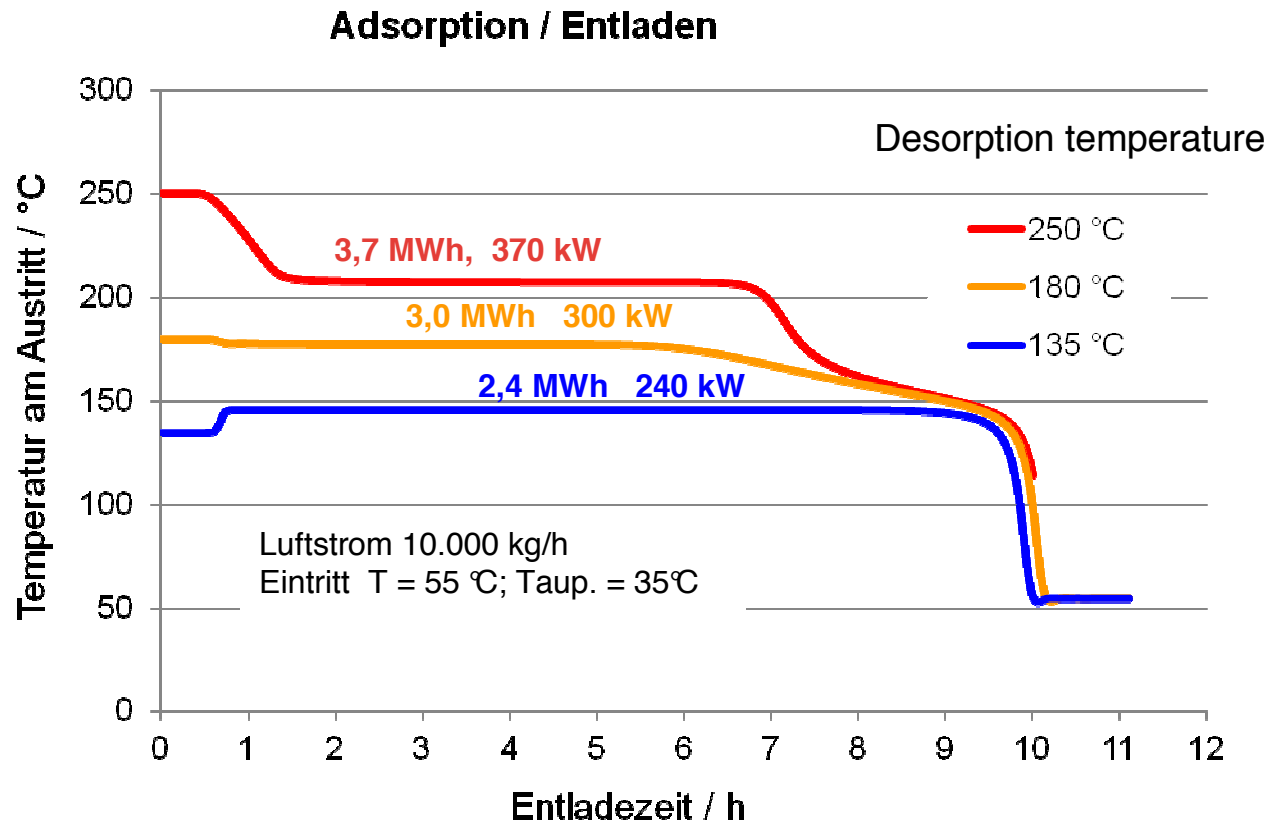
- Long time for charging
- Low power of charging

3. Example

3.4 Mobile Sorption Heat Storage - Simulation



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**Simulated Data
for ideal fixed
bed**

High desorption temperature:

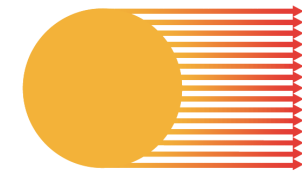
- High storage density
- High power of discharging

Low desorption temperature:

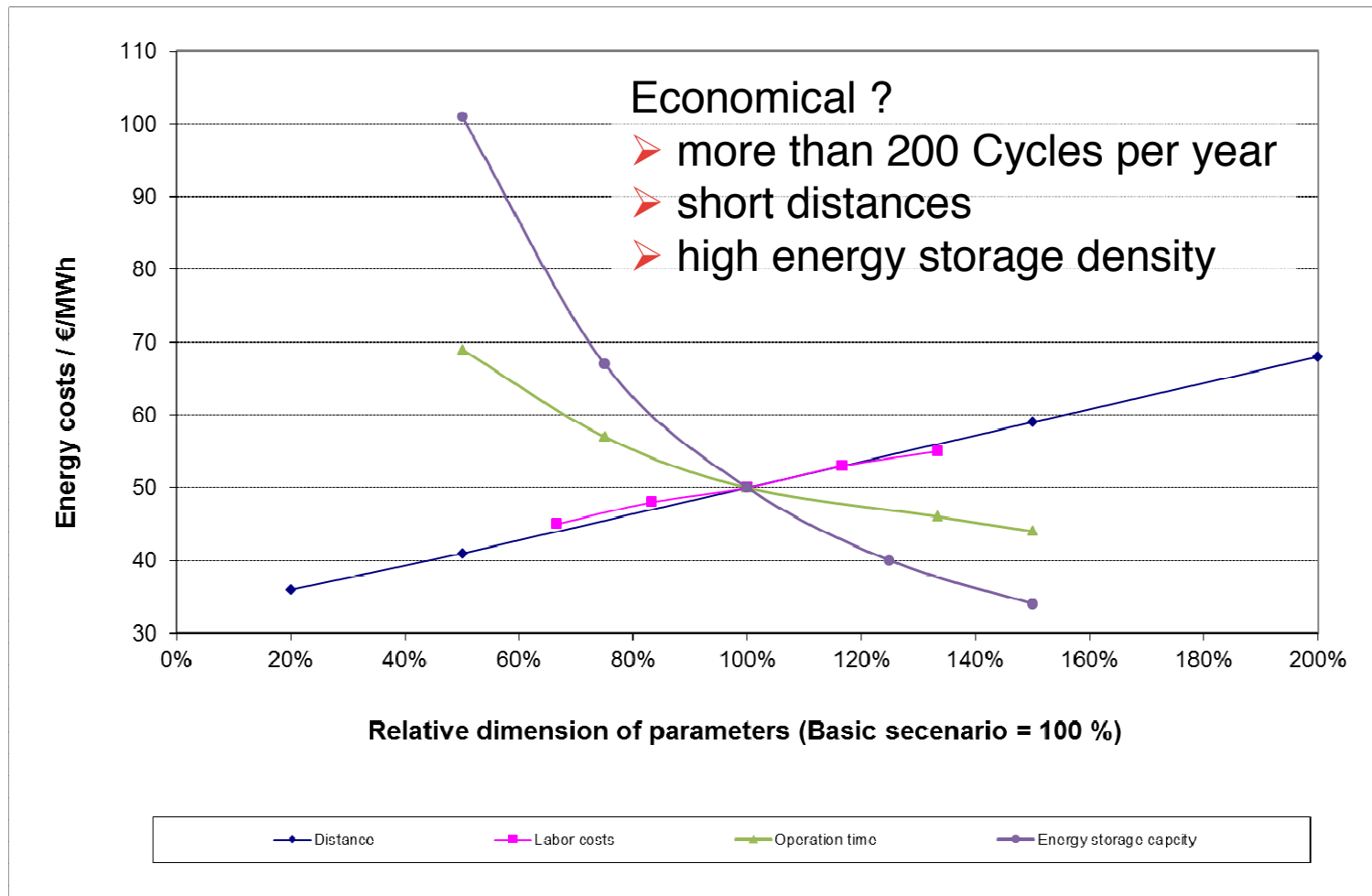
- Lower storage density
- Lower power of discharging

3. Example

3.5 Mobile Sorption Heat Storage – Study

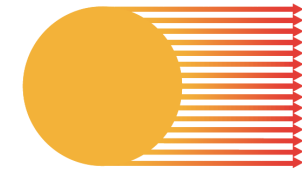


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3. Example

3.6 Mobile Sorption Heat Storage - Overview



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Parameter	Unit	Results
Storage Capacity	kWh/m ³	170 - 250 kWh/t 2,4 – 3,5 MWh
Charging Power Discharging Power	kW	250 – 800 kW 250 – 400 kW
Efficiency due to thermal losses	Energy charged / Energy discharged	0,9
Cycle time	h	Storage time: 1 h Cycle duration: 10 - 14 h
Economy	Heat generation costs	50 - 80 €/MWh

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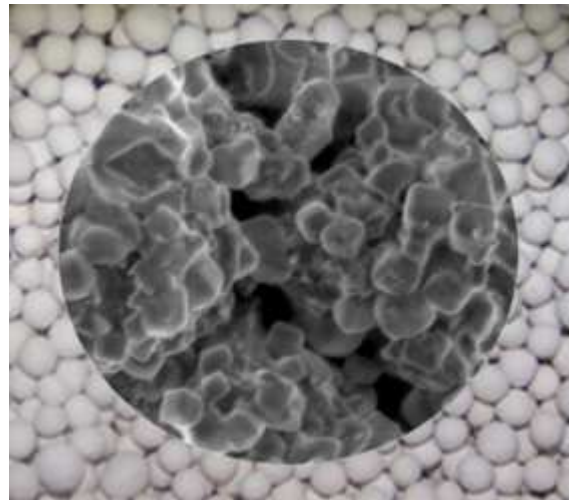


4. Summary



- Open adsorption storages can improve the energy efficiency
- Improvement of efficiency depends on the boundary conditions
- Drying processes in combination with waste heat processes are promising for sorption heat storages

Thank you very much for your attention!



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